

5.16 BOD<sub>5</sub>=180mg/L, k=0.22/day, TKN=30mg/L:

$$a. \text{CBOD} = L_0 = \frac{\text{BOD}_t}{(1 - e^{-kt})} = \frac{180}{(1 - e^{-0.22 \times 5})} = 270 \text{ mg/L}$$

$$b. \text{NBOD} = 4.57 \times \text{TKN} = 4.57 \times 30 \text{ mg/L} = 137 \text{ mg/L}$$

$$c. \text{BOD}_{\text{remaining}} = (270 + 137) - 180 = 227 \text{ mg/L}$$

5.18  $2 \text{CH}_2(\text{NH}_2)\text{COOH} + 3 \text{O}_2 \rightarrow 4 \text{CO}_2 + 2 \text{H}_2\text{O} + 2 \text{NH}_3$

$$\text{mol wt glycine} = 2 \times 12 + 5 \times 1 + 1 \times 14 + 2 \times 16 = 75 \text{ g/mol}$$

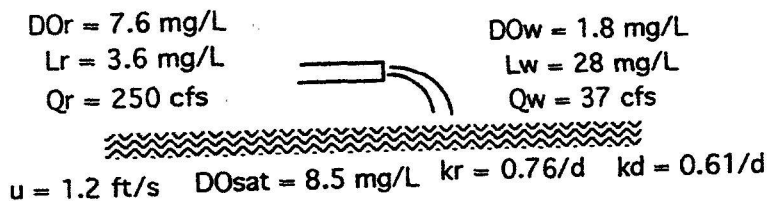
$$a. \text{CBOD} = \frac{3 \text{ mol O}_2}{2 \text{ mol glycine}} \times \frac{32 \text{ g O}_2 / \text{mol}}{75 \text{ g glycine/mol}} \times \frac{200 \text{ mg glycine}}{\text{L}} = 128 \text{ mg/L}$$

b. Nitrogenous portion:  $\text{NH}_3 + 2 \text{O}_2 \rightarrow \text{NO}_3^- + \text{H}^+ + \text{H}_2\text{O}$

$$\text{NBOD} = \frac{2 \text{ mol O}_2}{1 \text{ mol NH}_3} \times \frac{2 \text{ mol NH}_3}{1 \text{ mol glycine}} \times \frac{32 \text{ g/mol O}_2}{75 \text{ g/mol glycine}} \times \frac{200 \text{ mg glycine}}{\text{L}} = 171 \text{ mg/L}$$

$$c. \text{Total theoretical oxygen demand} = 128 + 171 = 299 \text{ mg/L}$$

5.30



a. initial conditions:

$$DO = \frac{37 \text{ cfs} \times 1.8 \text{ mg/L} + 250 \text{ cfs} \times 7.6 \text{ mg/L}}{37 + 250 \text{ cfs}} = 6.85 \text{ mg/L}$$

$$\text{Initial deficit} = D_0 = 8.5 \text{ mg/L} - 6.85 \text{ mg/L} = 1.65 \text{ mg/L}$$

$$\text{Initial BOD} = L_0 = \frac{37 \text{ cfs} \times 28 \text{ mg/L} + 250 \text{ cfs} \times 3.6 \text{ mg/L}}{37 + 250 \text{ cfs}} = 6.75 \text{ mg/L}$$

b. critical point:

$$t_c = \frac{1}{k_r - k_d} \ln \left( \frac{k_r}{k_d} \left[ 1 - \frac{D_0(k_r - k_d)}{k_d L_0} \right] \right)$$

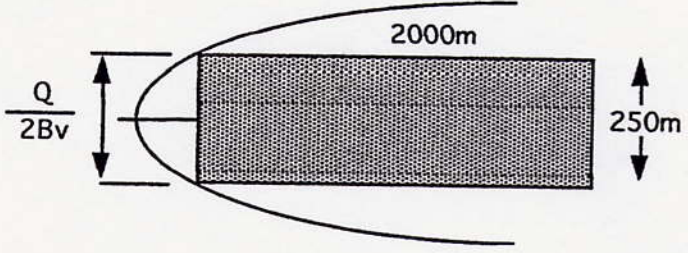
5.50  $0.1\text{m}^3$  TCE plume,  $B=10\text{m}$ ,  $2000\text{m} \times 250\text{m}$ ,  $\text{grad}=0.001$ ,  $K=0.001\text{m/s}$ ,  $h=0.4$ :

a. Can it dissolve? Using the specific gravity given in Table 5.15, the concentration  $C$  of TCE in the plume (if it could all dissolve) would be

$$C = \frac{0.1\text{m}^3 \times 1.47 \text{ kg/L} \times 10^3 \text{ L/m}^3 \times 10^6 \text{ mg/kg}}{2000\text{m} \times 250\text{m} \times 10\text{m} \times 0.40 \times 10^3 \text{ L/m}^3} = \frac{1.47 \times 10^8 \text{ mg}}{2 \times 10^9 \text{ L}} = 0.073 \text{ mg/L}$$

Since the solubility (Table 5.15) is  $1100 \text{ mg/L}$ , YES it could all dissolve.

b. Try a single well:



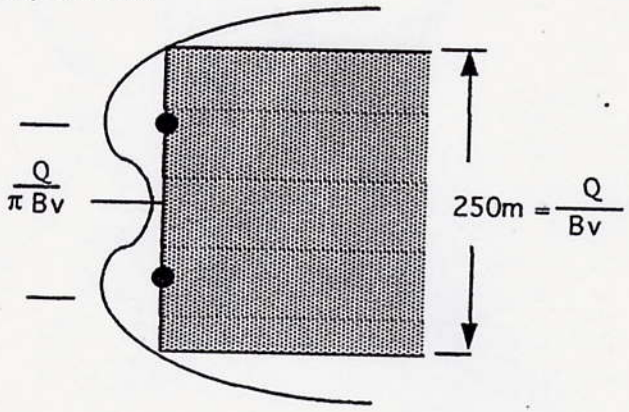
$$\frac{Q}{Bv} = 250\text{m}$$

$$v = K \frac{dh}{dL} = 0.001\text{m/s} \times 0.001 = 1 \times 10^{-6} \text{ m/s}$$

$$Q = 250 \times 2Bv = 250\text{m} \times 2 \times 10\text{m} \times 1 \times 10^{-6} \text{ m/s} = 0.005 \text{ m}^3/\text{s}$$

this exceeds the maximum pumping rate, which is given as  $0.003 \text{ m}^3/\text{s}$ .

Try 2 wells:



$$\frac{Q}{Bv} = 250\text{m}$$

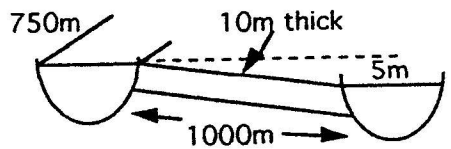
$$Q = 250\text{m} \times 10\text{m} \times 1 \times 10^{-6} \text{ m/s} = 0.0025 \text{ m}^3/\text{s} < 0.003 \text{ m}^3/\text{s}$$

so, 2 wells will work.

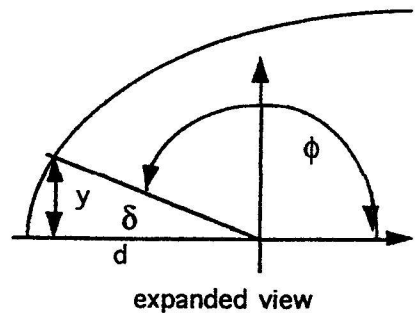
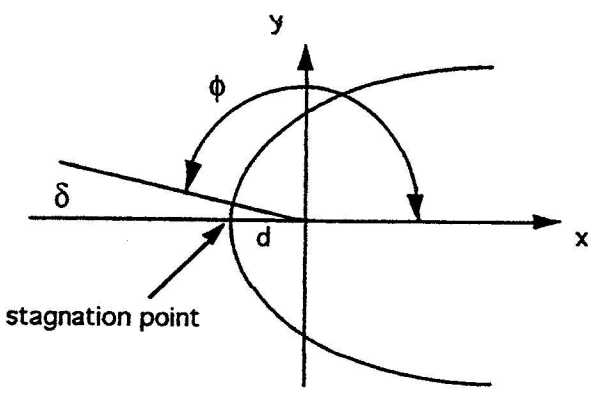
c. spacing for minimum pumping rate:

$$\text{spacing} = \frac{Q}{\pi Bv} = \frac{0.0025 \text{ m}^3/\text{s}}{\pi \times 10\text{m} \times 10^{-6} \text{ m/s}} = 79.6 \approx 80\text{m apart}$$

5.42



$$Q = KA \frac{dh}{dL} = 7.0 \frac{\text{m}}{\text{day}} \times (10\text{m} \times 750\text{m}) \times \frac{5\text{m}}{1000\text{m}} = 262.5\text{m}^3 / \text{day}$$

5.49 Show  $d = Q/(2Bv\pi)$ 

$$y = \frac{Q}{2Bv} \left( 1 - \frac{\phi}{\pi} \right) \quad (5.60)$$

from expanded view,

$$y = \frac{Q}{2Bv} \left[ 1 - \left( \frac{\pi - \delta}{\pi} \right) \right] = \frac{Q\delta}{2Bv\pi}$$

$$\left( \frac{y}{d} \right) = \tan \delta \approx \delta \text{ for small values of } \delta$$

Therefore, for small  $\delta$ ,  $y \approx \frac{Q}{2Bv\pi} \left( \frac{y}{d} \right)$ 

$$\text{so, } d = \frac{Q}{2Bv\pi}, \text{ that is, } x = -\frac{Q}{2Bv\pi} \quad \text{Q.E.D.}$$

$$= \frac{1}{0.76 - 0.61/d} \ln \left( \frac{0.76}{0.61} \left[ 1 - \frac{1.65(0.76 - 0.61)}{0.61 \times 6.75} \right] \right) = 1.05 \text{ days}$$

critical distance =  $x_c = 1.2 \frac{\text{ft}}{\text{s}} \times 3600 \frac{\text{s}}{\text{hr}} \times 24 \frac{\text{hr}}{\text{d}} \times 5280 \frac{\text{ft}}{\text{mi}} \times 1.05 \text{ day} = 20.7 \text{ miles}$

c. minimum DO:

$$D_{\max} = \frac{k_d L_0}{k_r - k_d} (e^{-k_d t} - e^{-k_r t}) + D_0 e^{-k_r t}$$

$$= \frac{0.61/d \times 6.75 \text{ mg/L}}{(0.76 - 0.61)/d} (e^{-0.61 \times 1.05} - e^{-0.76 \times 1.05}) + 1.65 e^{-0.76 \times 1.05} = 2.85 \text{ mg/L}$$

$DO_{\min} = DO_{\text{sat}} - D_{\max} = 8.5 - 2.85 = 5.6 \text{ mg/L}$

d. 10 miles downstream:

$$t = \frac{10 \text{ mi} \times 5280 \text{ ft/mi}}{1.2 \text{ ft/s} \times 3600 \text{ s/hr} \times 24 \text{ hr/d}} = 0.51 \text{ days}$$

$$D = \frac{k_d L_0}{k_r - k_d} (e^{-k_d t} - e^{-k_r t}) + D_0 e^{-k_r t}$$

$$= \frac{0.61 \times 6.75}{0.76 - 0.61} (e^{-0.61 \times 0.51} - e^{-0.76 \times 0.51}) + 1.65 e^{-0.76 \times 0.51} = 2.6 \text{ mg/L}$$

$DO = 8.5 - 2.6 = 5.9 \text{ mg/L}$

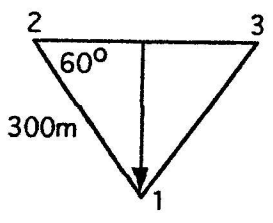
5.41 From Prob. 5.39,

grad = 0.00115, hydraulic conductivity  $K = 1000 \text{ m/d}$ , porosity = 0.23

a. Darcy velocity =  $v = K \frac{dh}{dL} = 1000 \text{ m/d} \times 0.00115 = 1.15 \text{ m/day}$

b. avg. linear velocity =  $v' = \frac{\text{Darcy velocity}}{\text{porosity}} = \frac{1.15 \text{ m/day}}{0.23} = 5.0 \text{ m/day}$

c.



without accounting for retardation,  $t = \frac{\text{distance, } d}{\text{avg. velocity } v'} = \frac{300 \sin 60^\circ}{5.0 \text{ m/day}} = 52 \text{ days}$

with retardation factor of 2:  $t = R \times 52 \text{ d} = 2 \times 52 \text{ d} = 104 \text{ days}$